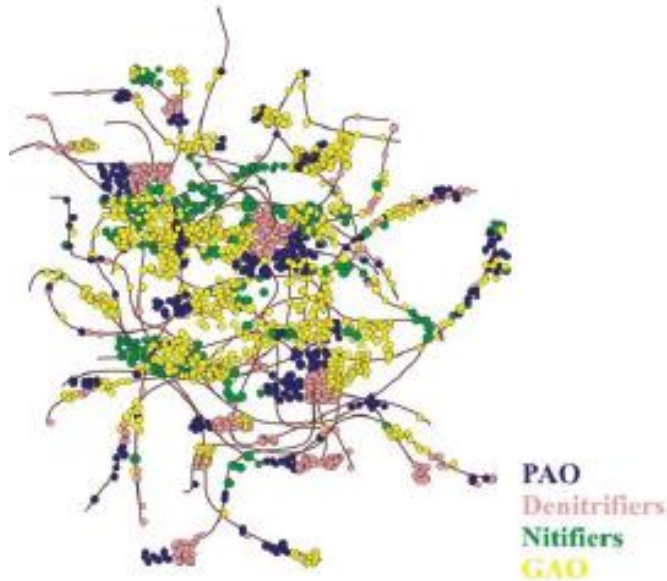


Hazen



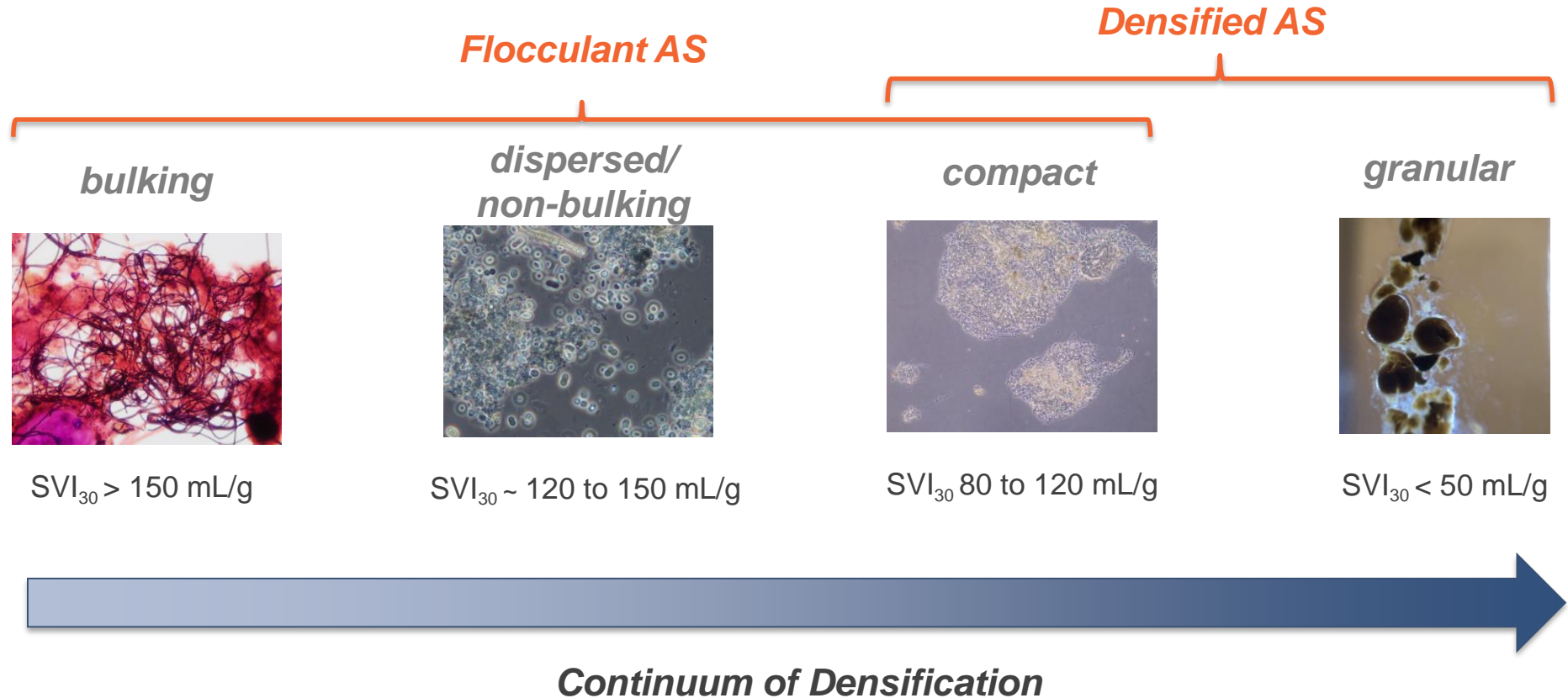
The Value of Metabolic Selection in the Pursuit of Densified Activated Sludge

TACWA January 31, 2020

Outline

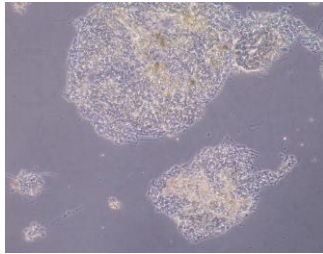
- What is densified sludge?
- Metabolic selection
- Benefits of densification
- How can we achieve densification?
- Case studies
- How densification impact plant capacity?
- Conclusions

What Is Densified Activated Sludge (DAS)?

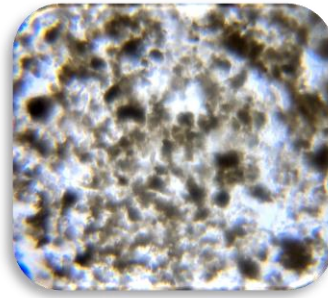


How Does DAS Compare with Granular Sludge?

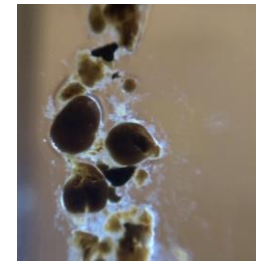
*Compact AS
(non-granular)*



*Densified AS
(non-granular)*



*Densified AS
(granular)*



non-patented AS
Conventional
Selector Design

non-patented AS*

AquaNEREDA™
inDENSE™

How do we Bridge the Gap?

Metabolic Selection For Improving Settleability Is Not New...

- Chudoba et al. (1973, 1984)
 - Presented kinetic selection theory based on monod
- Van Niekerk et al. (1988)
 - Eq. to determine selector hydraulic detention time
- Multitude of publications
- Design guidelines target F:M ratios and HRTs
- In absence of historical data ***an SVI of 150 mL/g should be used if the facility uses selectors***

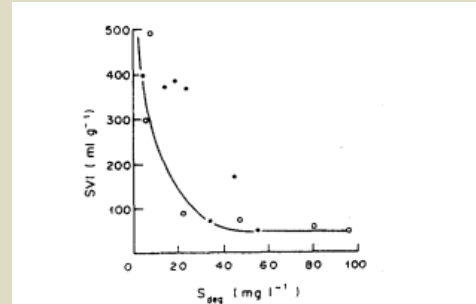
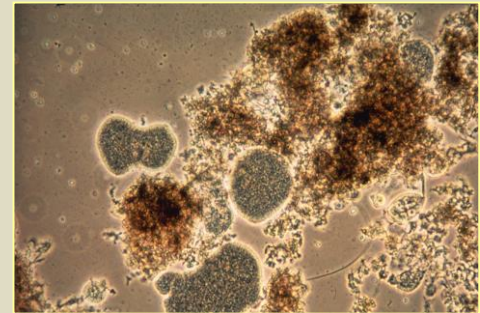
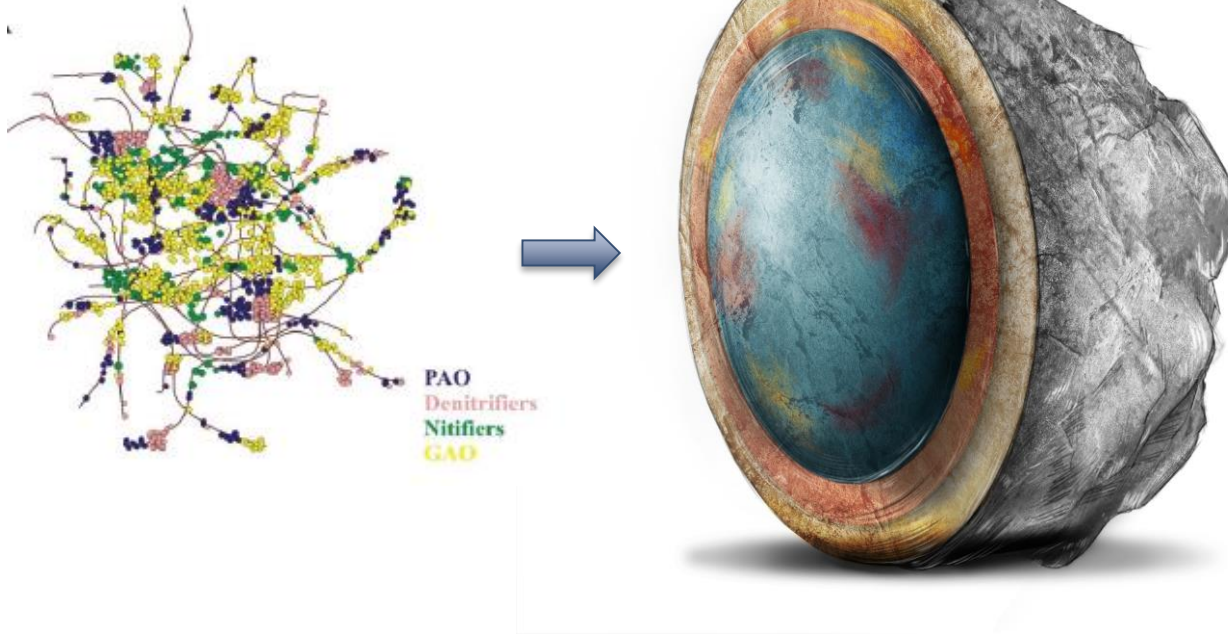


Fig. 7. Relationship between SVI and soluble degradable COD in the first selector compartment. ○ Chudoba et al. (1973a, b); ● Lee et al. (1982).



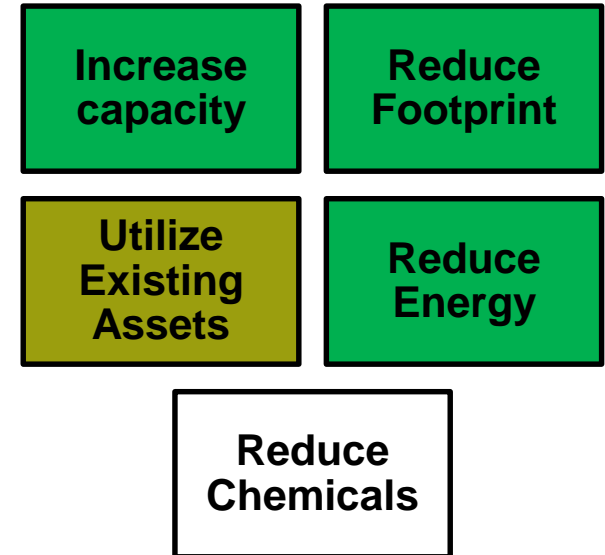
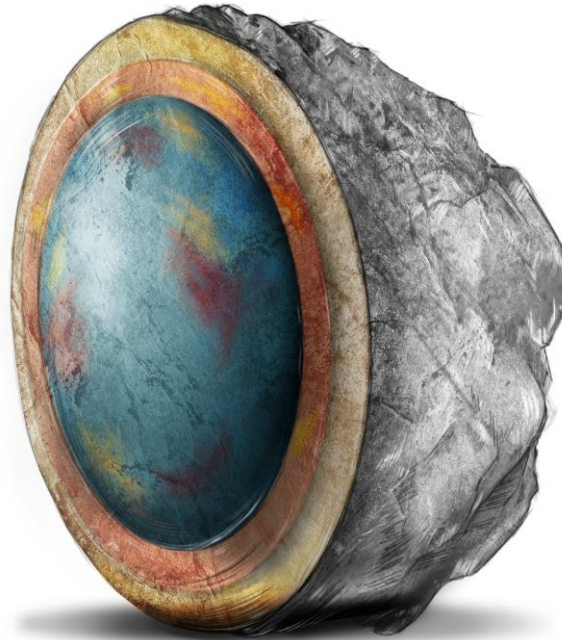
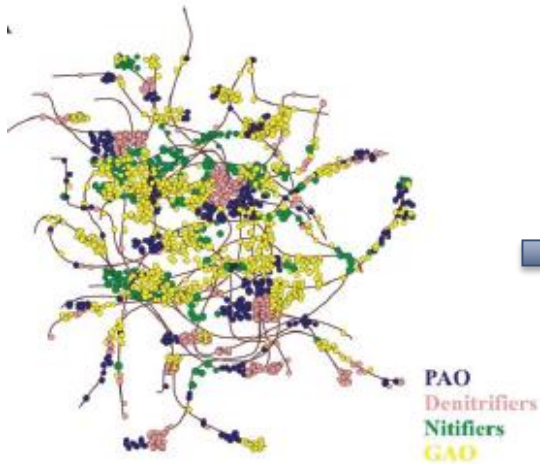
*Why Achieve
Densification?*

DAS Is An Enhancement to Activated Sludge that Facilitates Rapid Settling



Underlying benefit is due to improved settleability

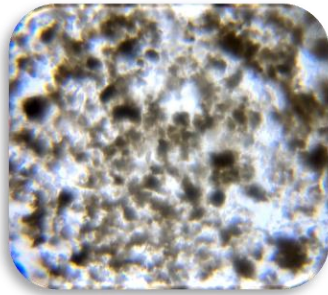
DAS Is Key to Unlocking Capacity at WRRFs



*How Do We Achieve
Densification?*

Non-granular DAS Possesses Enhanced Settling Properties Versus Conventional Activated Sludge

Non-granular DAS



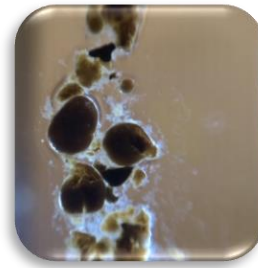
$SVI_{30} < 70 \text{ mL/g}$

$SVI_{10} \sim SVI_{30}$

Particle size $< 212 \text{ } \mu\text{m}$

Effluent TSS $< 4 \text{ to } 10 \text{ mg/L}$

granular sludge



$SVI_{30} < 50 \text{ mL/g}$

$SVI_5 \sim SVI_{30}$

Particle size $> 212 \text{ } \mu\text{m}$

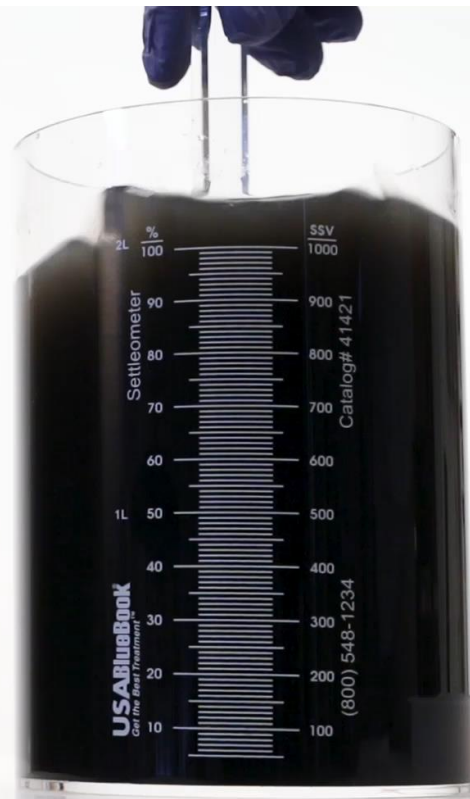
Effluent TSS $\sim 8 \text{ to } 15 \text{ mg/L}$

Non-granular DAS
MLSS _ 2,700 mg/L
SVI5 ~ 52 mL/g
SVI30 ~ 50 mL/g

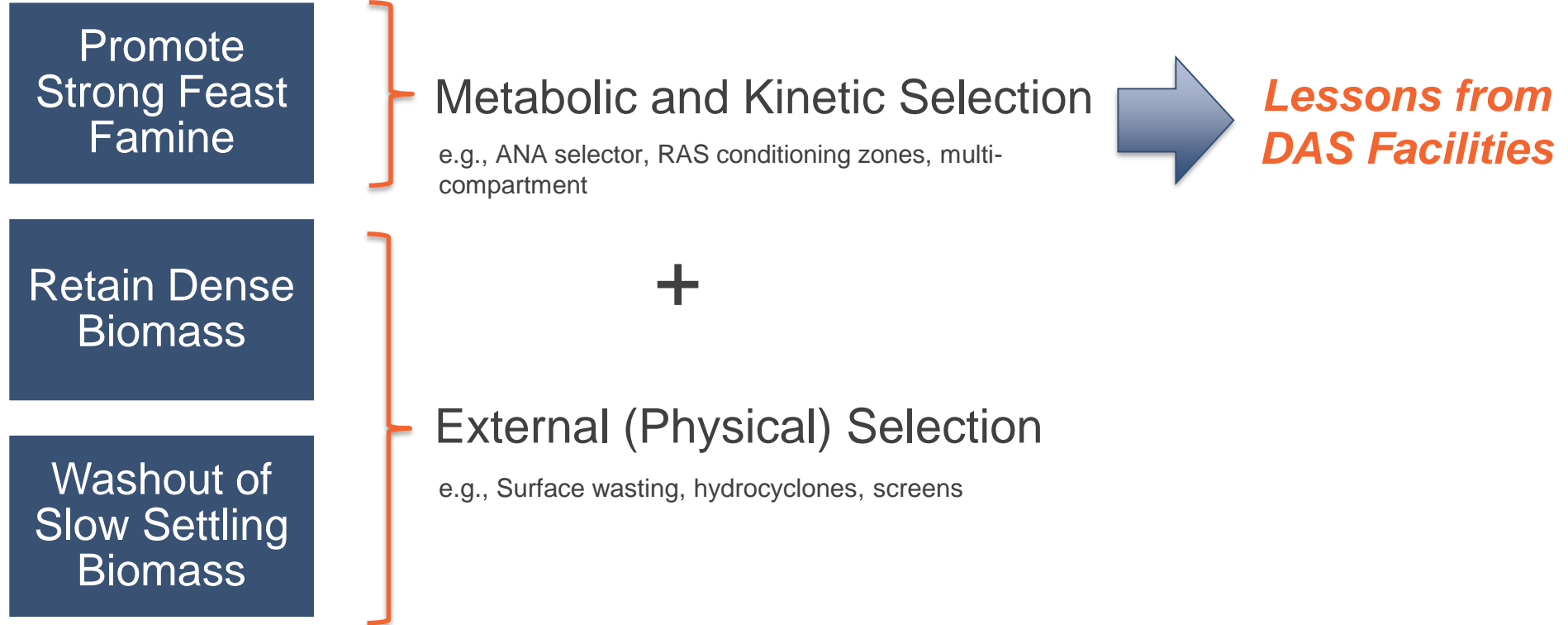


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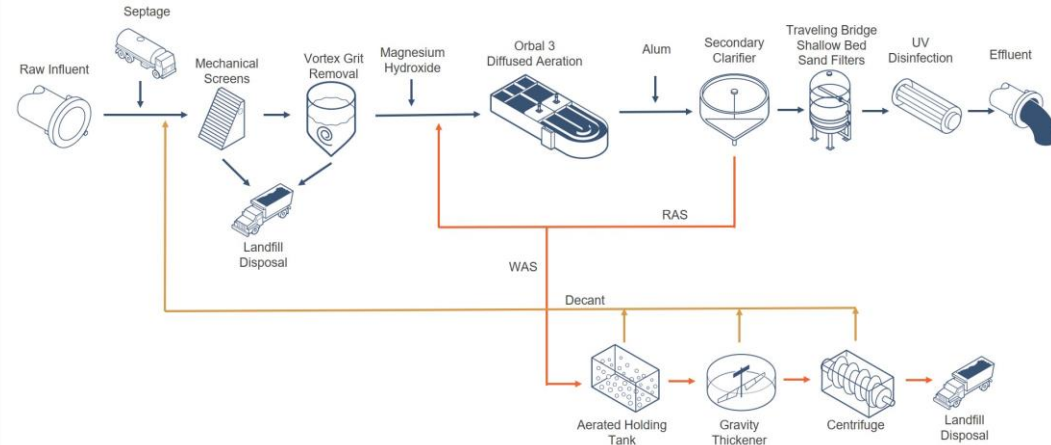
Flocculant AS
MLSS _ 3,000 mg/L
SVI5 ~ 250 mL/g
SVI30 ~ 175 mL/g



What Are the Ingredients to Achieve Densified Activated Sludge (DAS)?

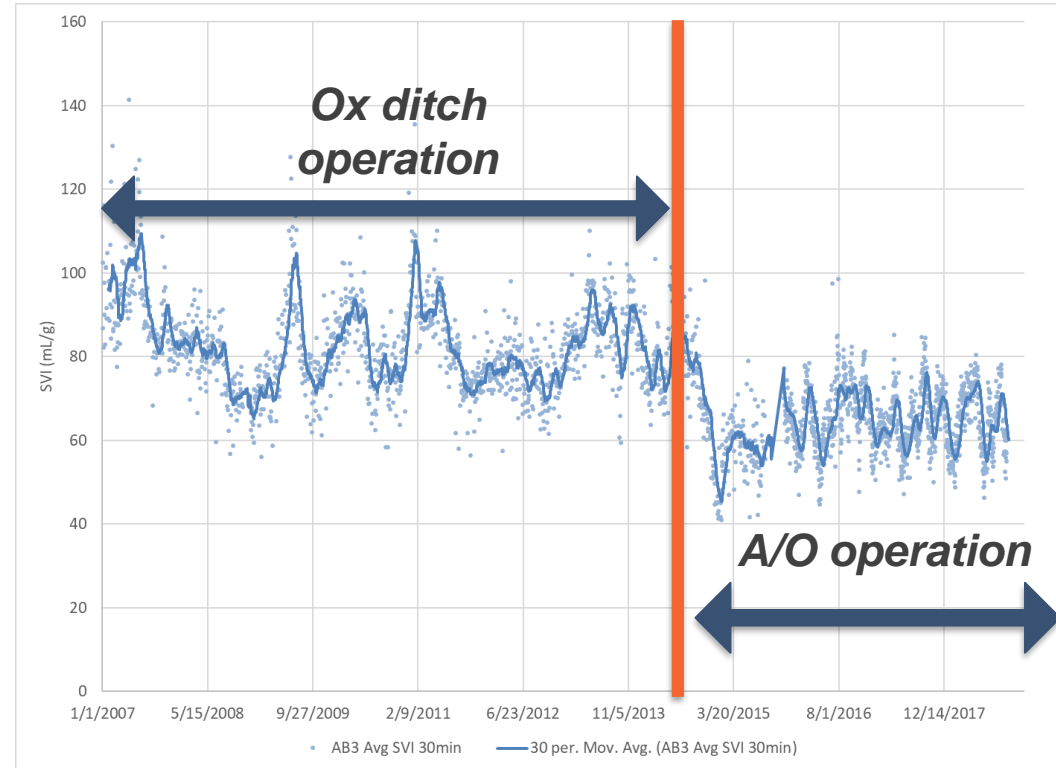


Plant A – Metabolic Selection In A/O Process



Plant A Settling Improved Once Diffused Aeration Upgrade Completed

- 10 mgd MM capacity
- Operating at 7 mgd
- A/O process in Orbal retrofit with diffused aeration
- Current performance targets
 - $NH_3-N < 1 \text{ mg/L}$
 - $TP < 0.5 \text{ mg/L}$



Plant A Biomass Settling Properties Approach Those Observed for Lab-Scale AGS

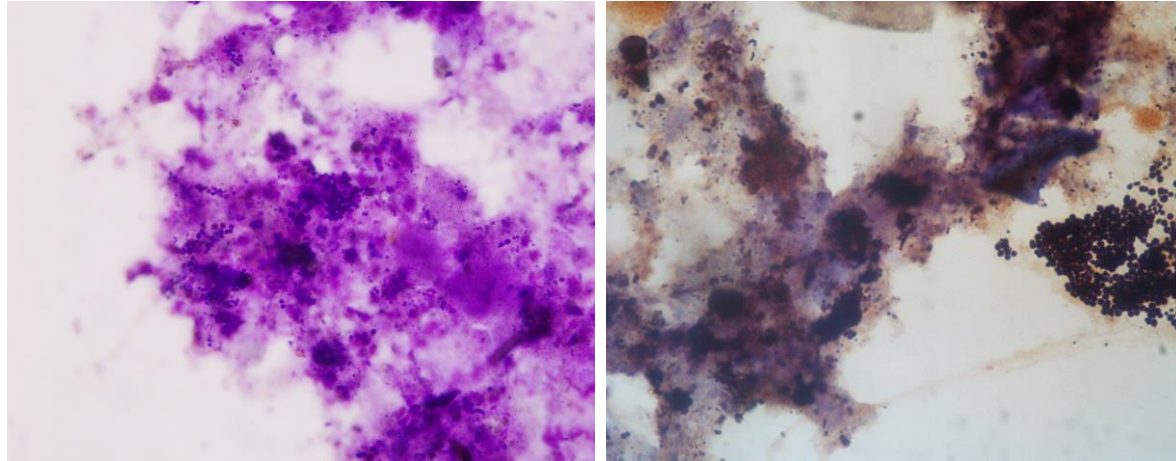


SVI5 ~ 75 mL/g
SVI30 ~ 64 mL/g

SVI5 ~ 58 mL/g
SVI30 ~ 45 mL/g

	Vo ft/hr	K L/g
Conventional Activated Sludge	30 to 38	0.4 to 0.8
Plant A DAS		

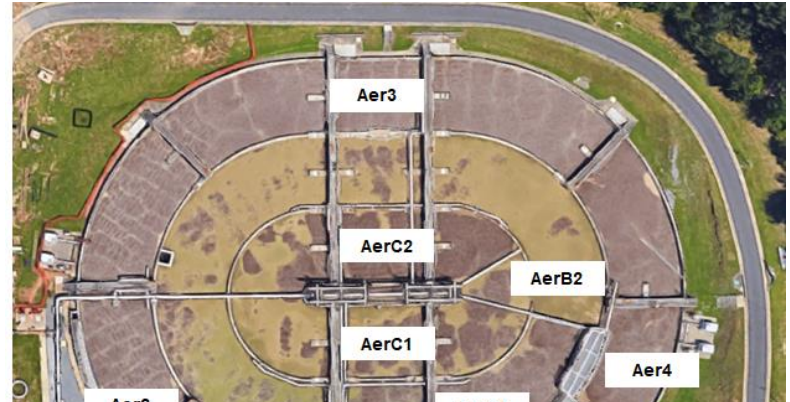
Plant A Biomass Distribution Indicates ~ 50% of Biomass > 212 um



- Strong PAO population observed
- Nocardioform type organisms also present

Influent and Recycle Characteristics

- Inf sCOD ~ 30% of influent tCOD
- Relatively high F/M experienced throughout anaerobic zone



The Impact of Applying an Internal Substrate Selection Strategy to Improve Aerobic Granular Sludge Formation

Authors: Rasha Faraj^{1*}, Theresa Amante¹, Jennifer Warren¹, Mariela Mosquera¹, and Belinda Sturm¹

¹Department of Civil, Environmental and Architectural Engineering, The University of Kansas, 1530 West 15th Street., Lawrence, KS 66045, USA

* Email: r410f839@ku.edu

Ana F/M > 0.2 g rbCOD/g VSS-day

What Might be Occurring at Plant A?

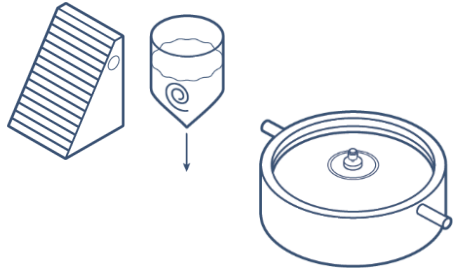
High organic loading
due to favorable
influent characteristics

Low $\text{NO}_3\text{-N}$ in RAS
results in minimal
denite demand in Ana
zones

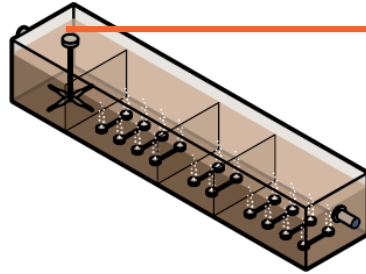
Stratification of
biomass in Ana zones
may result in
fermentation

*Plant C –
Nitrified Activated
Sludge with Selector*

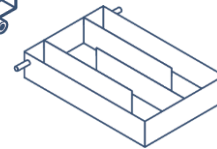
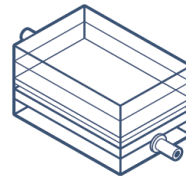
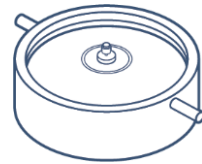
Pant C Configuration



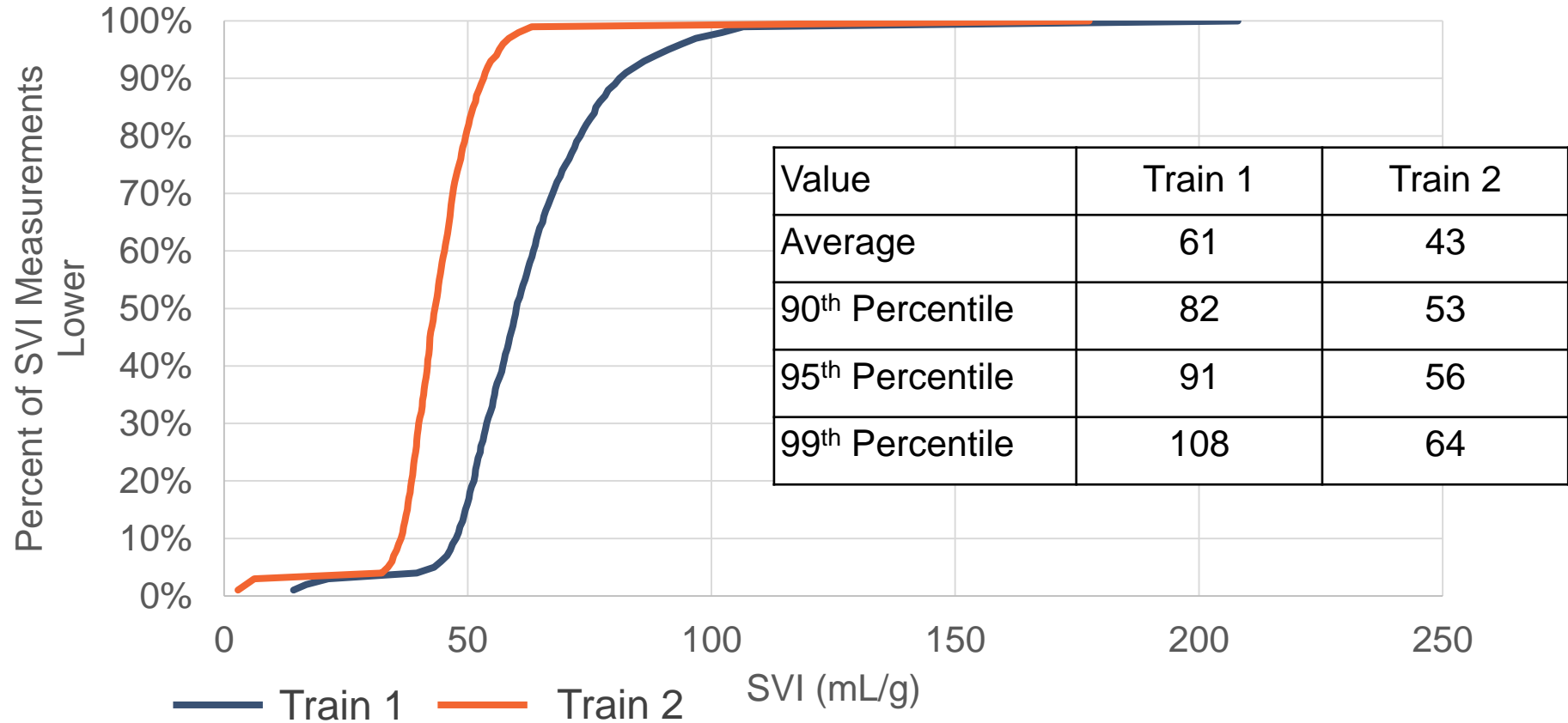
- 24 mgd AA capacity
- Operating at 15 mgd
- NAS with selector
- Current performance targets
 - $NH_3-N < 3 \text{ mg/L}$
 - $TP < 1.0 \text{ mg/L}$



Two Trains (similar volumes)
Train 1 – Low D.O. Selector
Train 2 – Mechanical Mixing

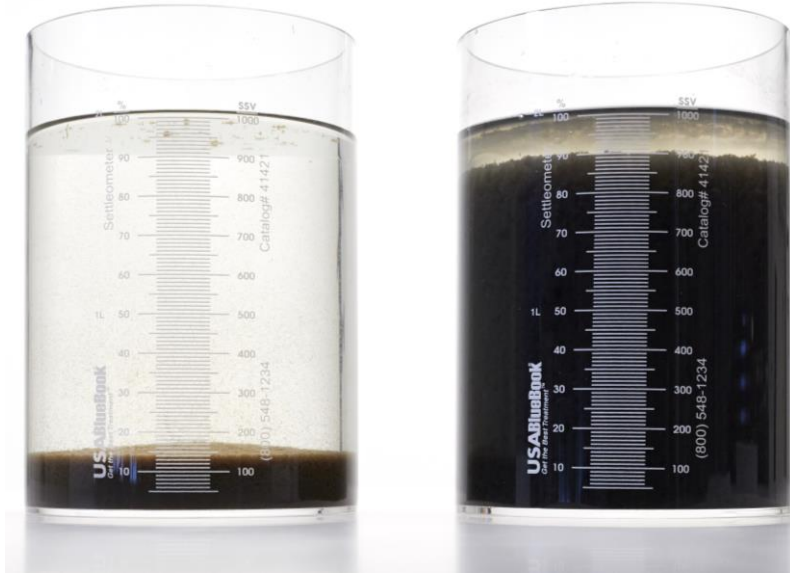


Historical SVI -Train 1 vs Train 2



Train 1 and 2 Biomass Settling Properties

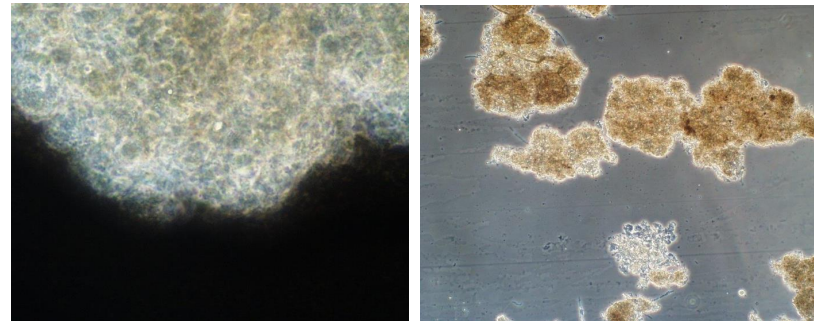
After 5 minutes of settling



Plant C
Train 2

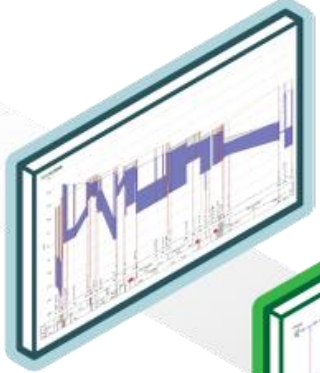
Conventional

	Vo ft/hr	K L/g
Conventional Activated Sludge	30 to 38	0.4 to 0.8
Plant A DAS		



**State-of-the-art tools
provide confident and
reliable solutions**

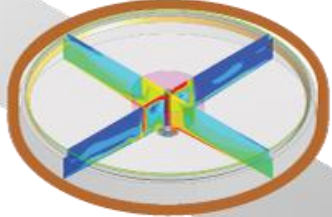
**Whole Plant
Hydraulic Models**



**WWTP
Process
Models**



**CFD
Clarifier
Models**

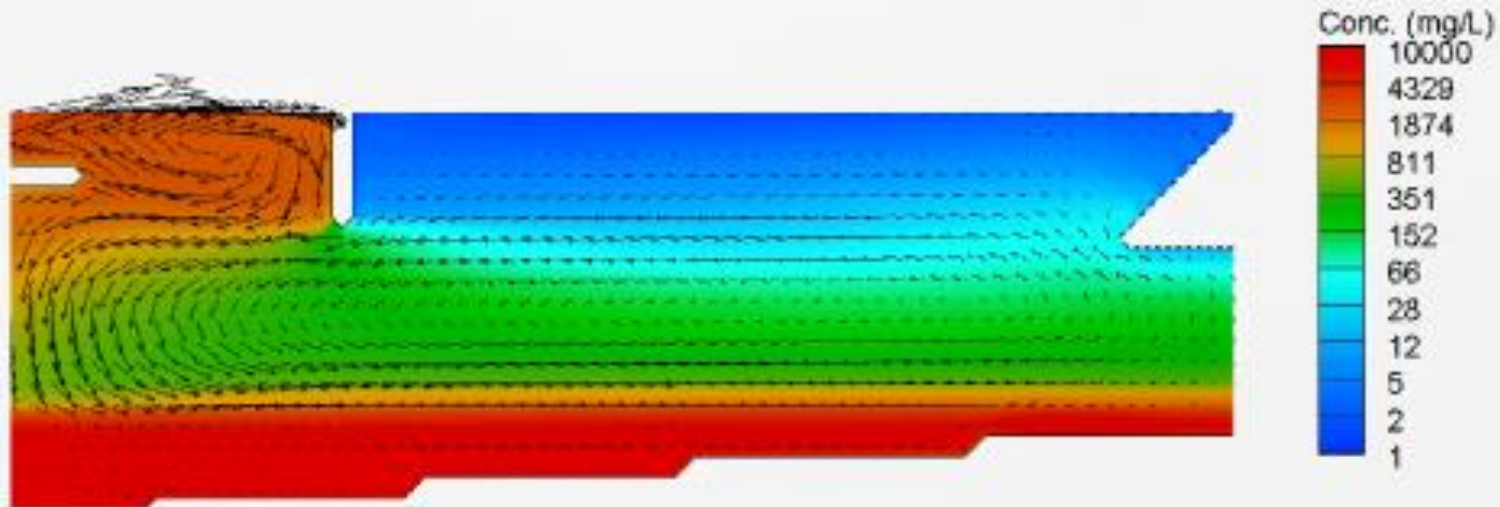


**Capacity
Analysis and
Optimization**

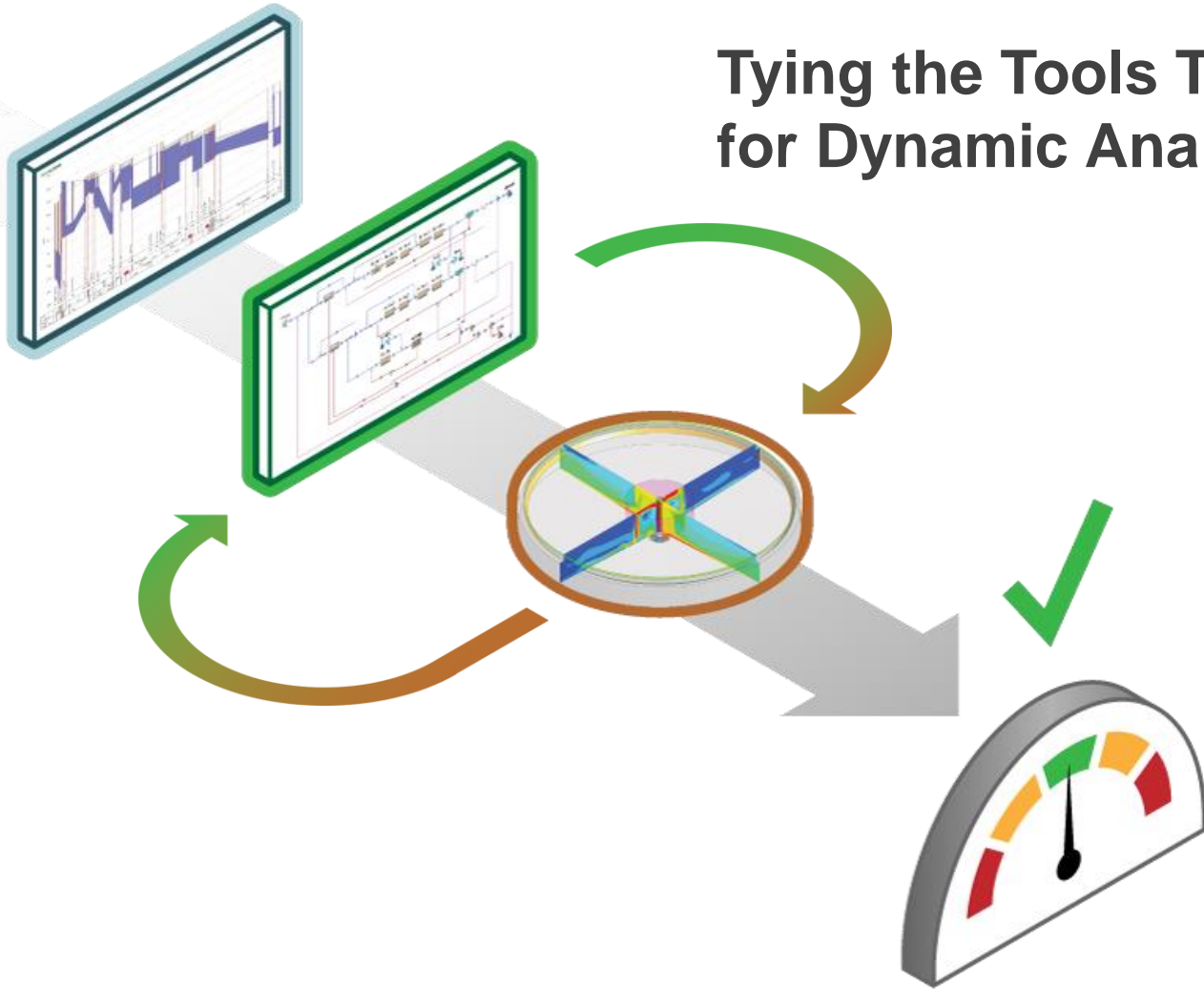
Plant C Dynamic Clarifier Simulation

Secondary Clarifiers 5 & 6
SVI = 100 mL/g (High Vo Factor)
Max SOR= 1,640 gp/d/sf
100% Step Feed Option

Results
Max ESS < 20 mg/L



Tying the Tools Together for Dynamic Analysis



**For Plant C analysis:
Confidently increase process
peak flow capacity by 40%**

Plant C Peak Flow Capacity Alternatives

Base Case – MBR conversion

Alternative 1 – DAS configuration with step feed flexibility

Alternative 2 – Wet weather biological high rate treatment system

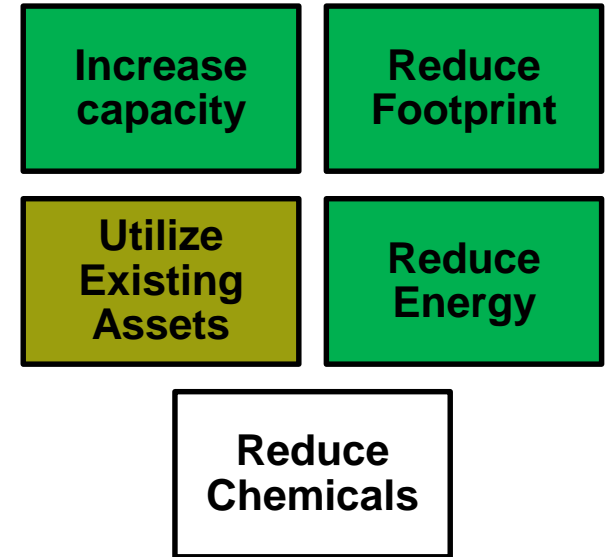
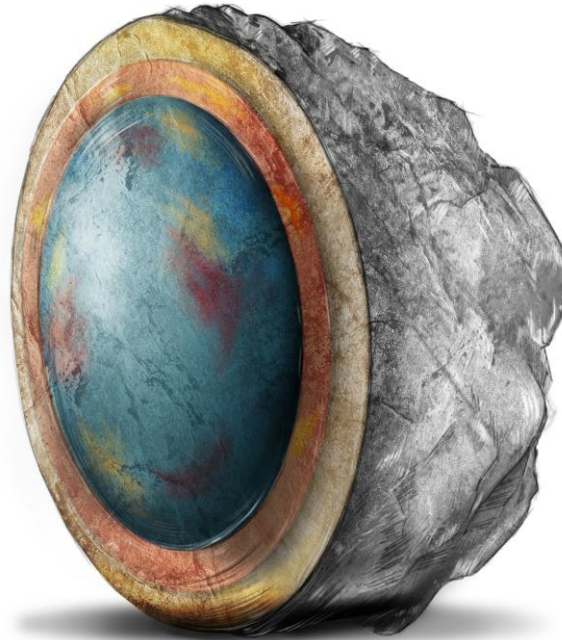
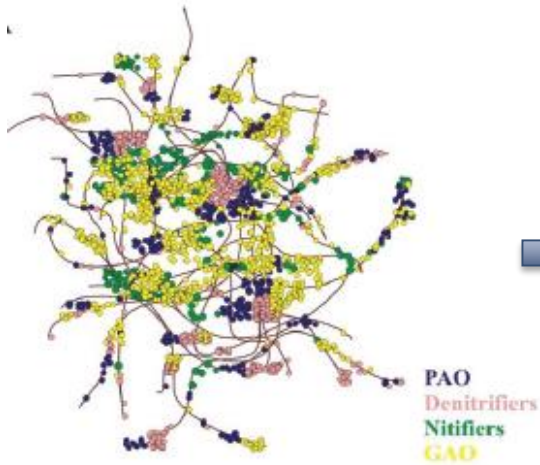
Cost Comparison

Alternatives	Capital Cost	20-Year O&M Present Value	Life Cycle Cost 20-Year NPV
Base Case: MBR Conversion	\$80M	\$60M	\$140M
1: DAS with step feed flexibility	\$60M	\$30M	\$90M
2: High rate wet weather treatment system	\$70M	\$35M	\$105M

\$20M savings
in liquid process improvements with
recommended alternative

Concluding Thoughts

DAS Is Key to Unlocking Capacity at WRRFs



DAS Can Be Achieved in Continuous Flow Configurations

Promote
Strong Feast
Famine

**Metabolic Selection might
be sufficient to achieve
non-granular DAS**

Retain
Dense
Biomass

**Physical selection may be
necessary for granule
morphology**

Washout of
Slow Settling
Biomass

Questions



Hazen

Paul Pitt
Wendell Khunjar
Alonso Griborio
Ron Latimer
Ankit Pathak
Rebecca Holgate



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